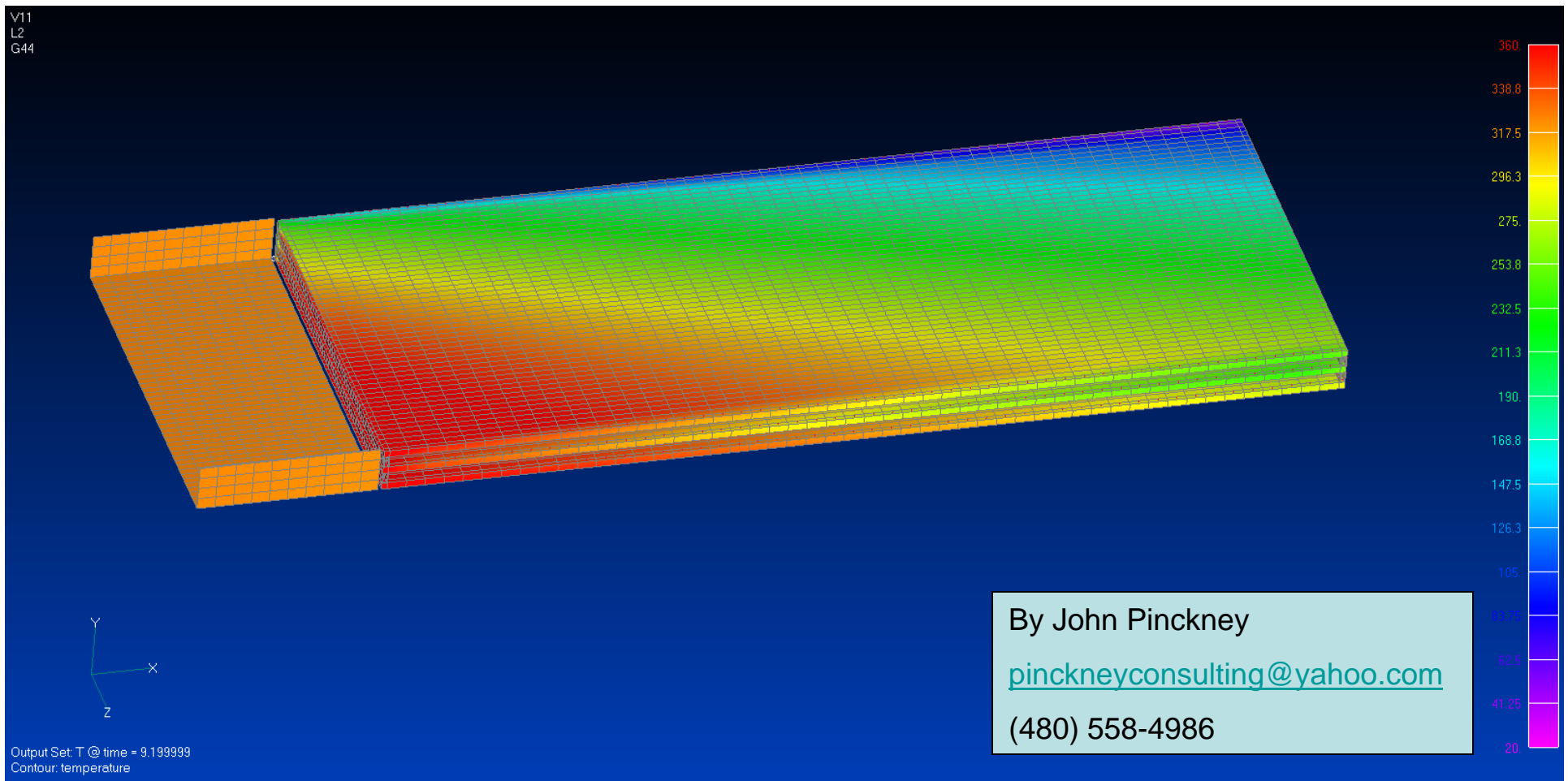


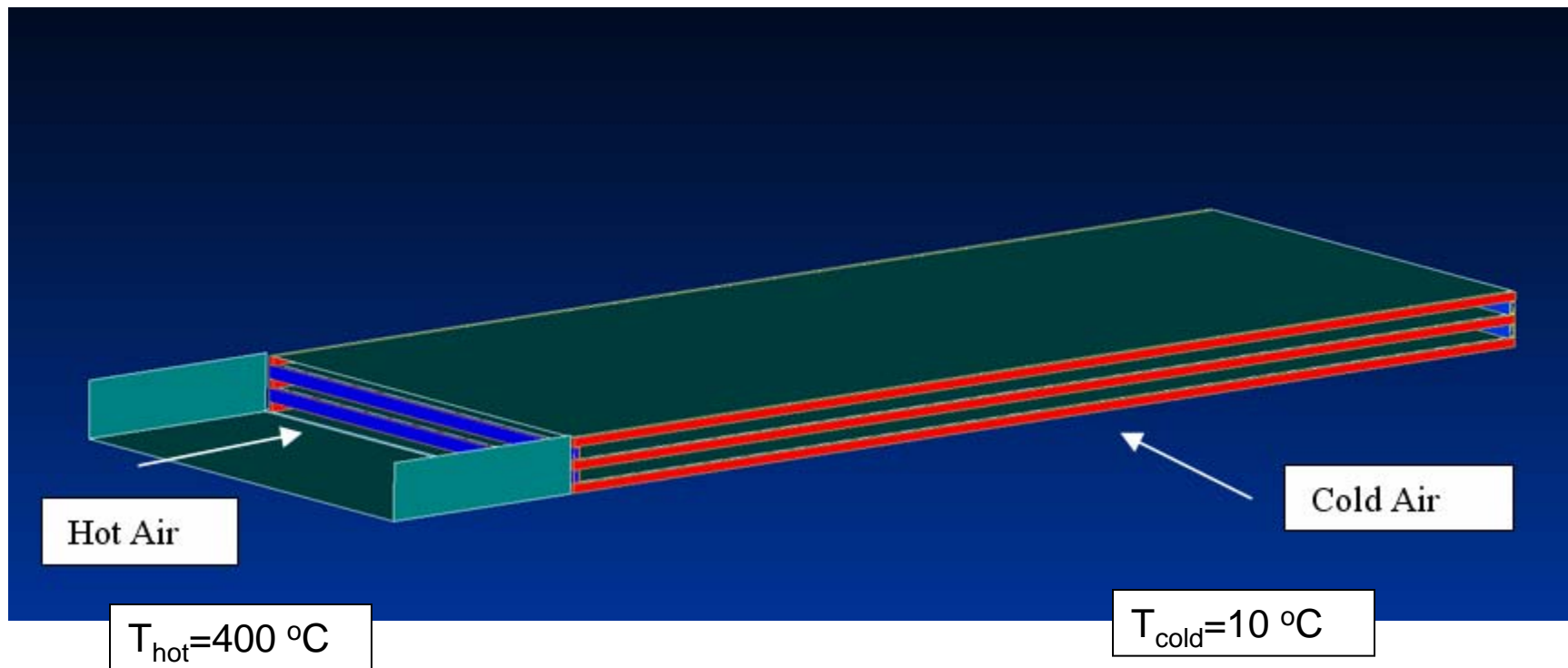
# Transient Thermal Analysis of Compact Cross Flow Heat Exchanger for Aviation Application

- Pulsed hot air operation
- Modeled using innovative technique of applying fin equations within *SINDA/G for Femap*
- Results used for performance and thermal stress analysis

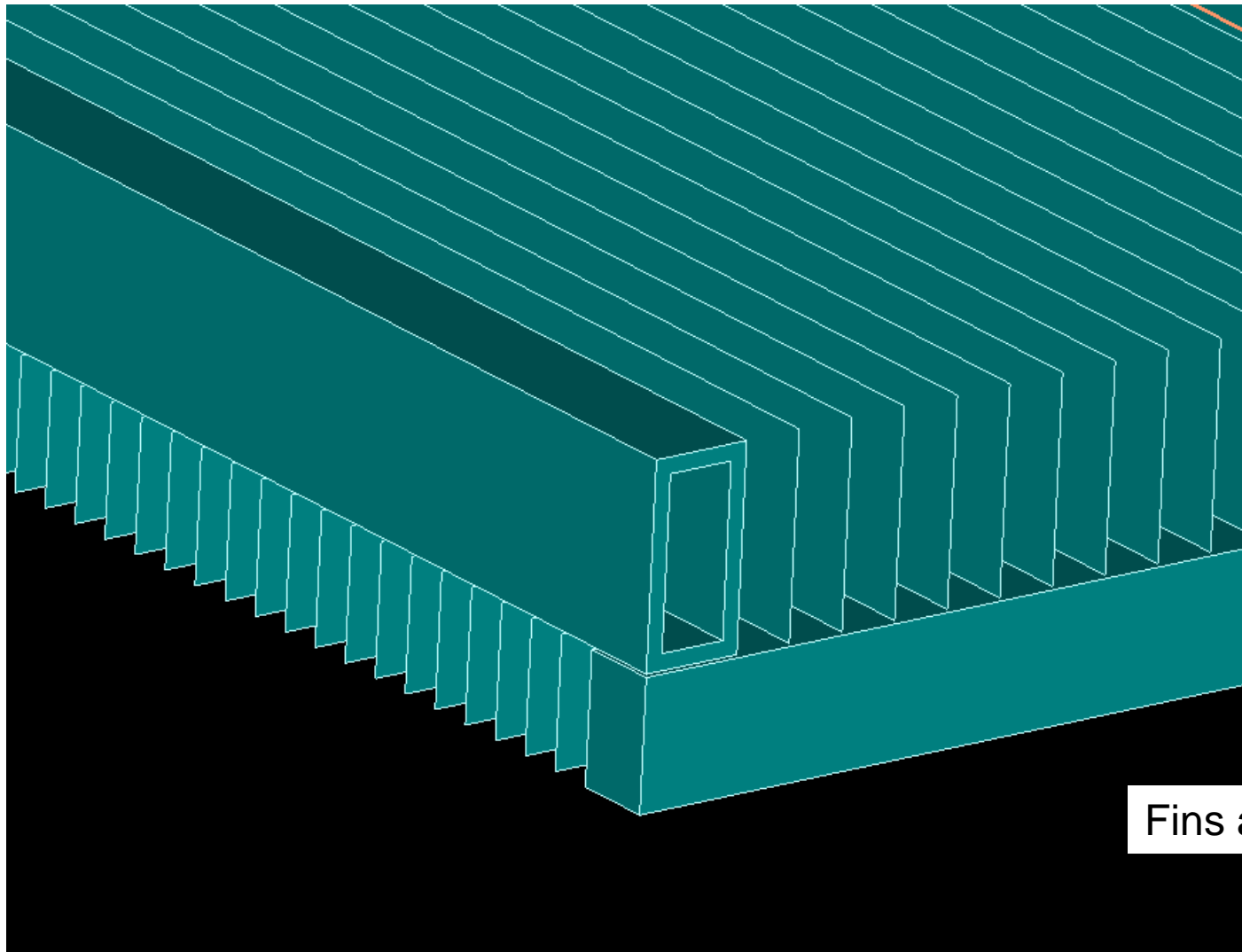


The heat exchanger is of a compact cross-flow finned and plate type consisting of  $n$  layers. Each layer consists of parallel parting sheets with parallel and evenly spaced fins placed perpendicular to the parting sheets. The layers are closed on two opposing edges by closure bars. The fins run in perpendicular directions in alternating layers. Hot air and cold air enter the heat exchanger in alternating layers resulting in perpendicular flow vectors.

Five Layers were modeled.



# Close up of a Hot and Cold Layer



Fin spacing is 1.44 mm for the hot layers and 1.8mm for the cold layers. The cold closure bars are hollow. (The fins were not in the actual *Femap* model.)

Fins are 0.05 mm thick.

# Super Fins

For modeling purposes fins were grouped into “Super Fins” and fin factors calculated for these Super Fins.

$\eta_{FinHot} := \frac{148}{0.214}$   
 $\eta_{FinCold} := \frac{290}{0.533}$

Fins per meter  
 $\eta_{FinHot} = 6.91589 \times 10^2$   
 $\eta_{FinCold} = 5.4409 \times 10^2$

$\delta_{fin} = 0.00005$   
 $\frac{1}{\eta_{FinHot}} = 1.44595 \times 10^{-3}$   
 $\frac{1}{\eta_{FinCold}} = 1.83793 \times 10^{-3}$

What fraction of parting surfaces covered by fins?

$\eta_{FinHot} \delta = 3.45794 \times 10^{-2}$   
 $\eta_{FinCold} \delta = 2.72045 \times 10^{-2}$

Hot Parting

What fraction of parting surfaces covered by fins?

$\eta_{FinHot} \delta = 3.45794 \times 10^{-2}$   
 $\eta_{FinCold} \delta = 2.72045 \times 10^{-2}$

+

$d_{hot1} := 0.0030988$   
 $d_{hot2} := 0.0041784$   
 $d_{hot3} := 0.010536$

$Fin_{factorhot1} := \eta_{FinHot} \cdot \frac{d_{hot2}}{2}$   
 $Fin_{factorhot2} := \eta_{FinHot} \cdot d_{hot2}$

$Fin_{factorhot1} = 1.44487 \times 10^0$   
 $Fin_{factorhot2} = 2.88973 \times 10^0$

$A_{hot2} := \frac{d_{hot1} \cdot d_{hot2}}{4}$   
 $d_{hot3} \cdot d_{hot2} = 4.40236 \times 10^{-5}$

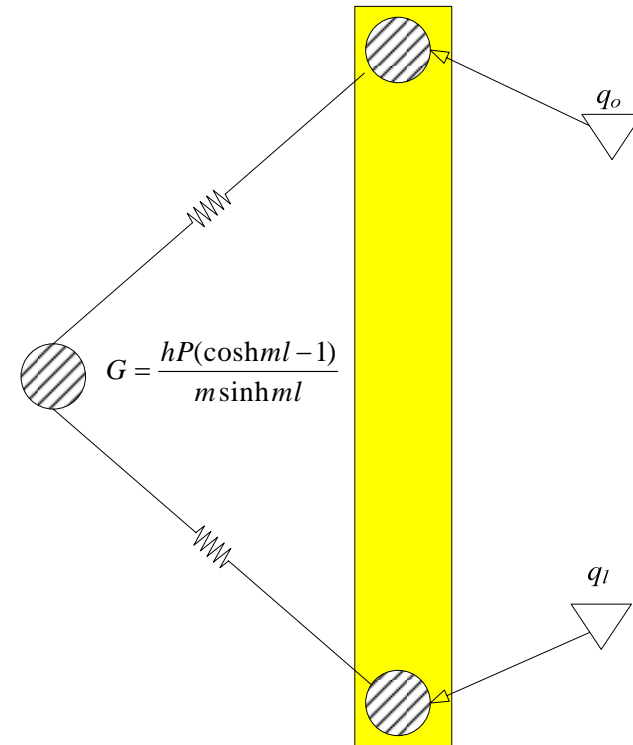
Super Fin sections modeled as three nodes with two conductors and two heat terms.

$$q_l = \frac{hP}{m \sinh ml} (\Theta_o \cosh ml - \Theta_l)$$

$$q_o = \frac{hP}{m \sinh ml} (\Theta_o - \Theta_l \cosh ml)$$

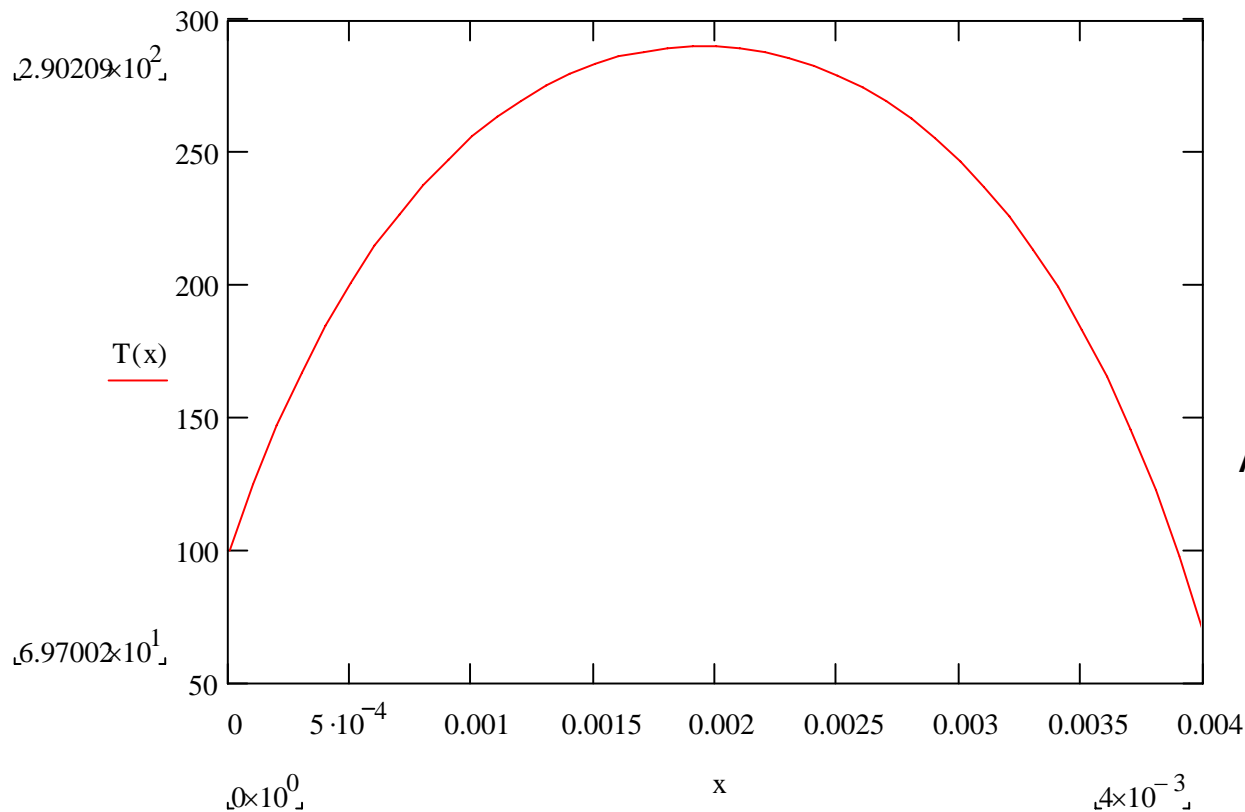
$$q_{con} = \frac{hP(\cosh ml - 1)}{m \sinh ml} (\Theta_o + \Theta_l)$$

See: *Fundamentals of Heat Exchanger Design*. Ramesh K. Shah, Dusan P. Sekulic. John Wiley & Sons, Hoboken, New Jersey. 2003



$\Theta$  is difference in temperatures between air stream and fin location.

The fin equations are necessary because large errors will result in the convective heat transfer calculations otherwise. It is impractical to mesh fins fine enough to accurately capture the fin temperature profile.

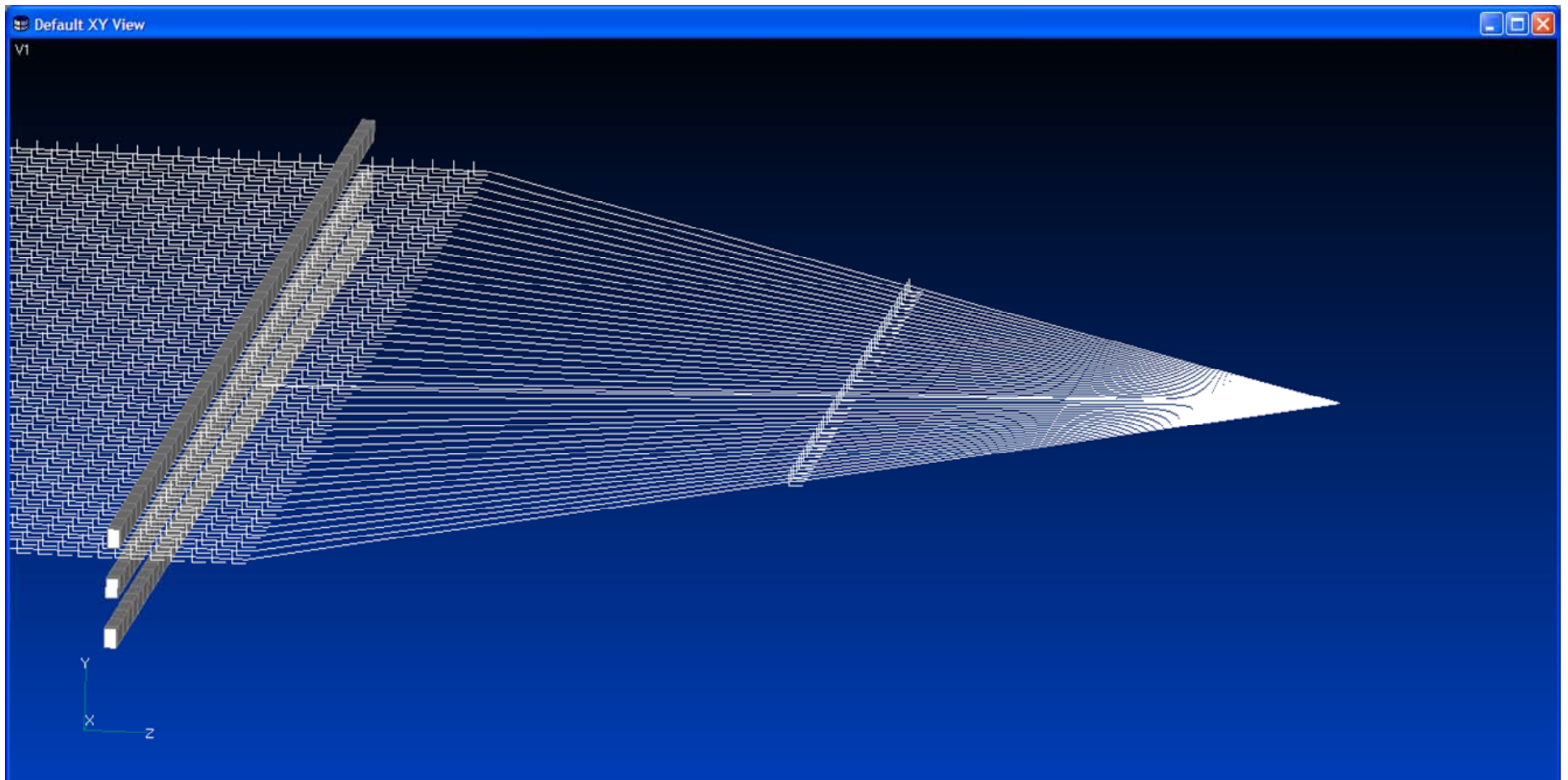


A fin temperature profile.

Custom Fortran code was written to find nodal relations, add heats, update convection conductors, simulate hot air pulse.

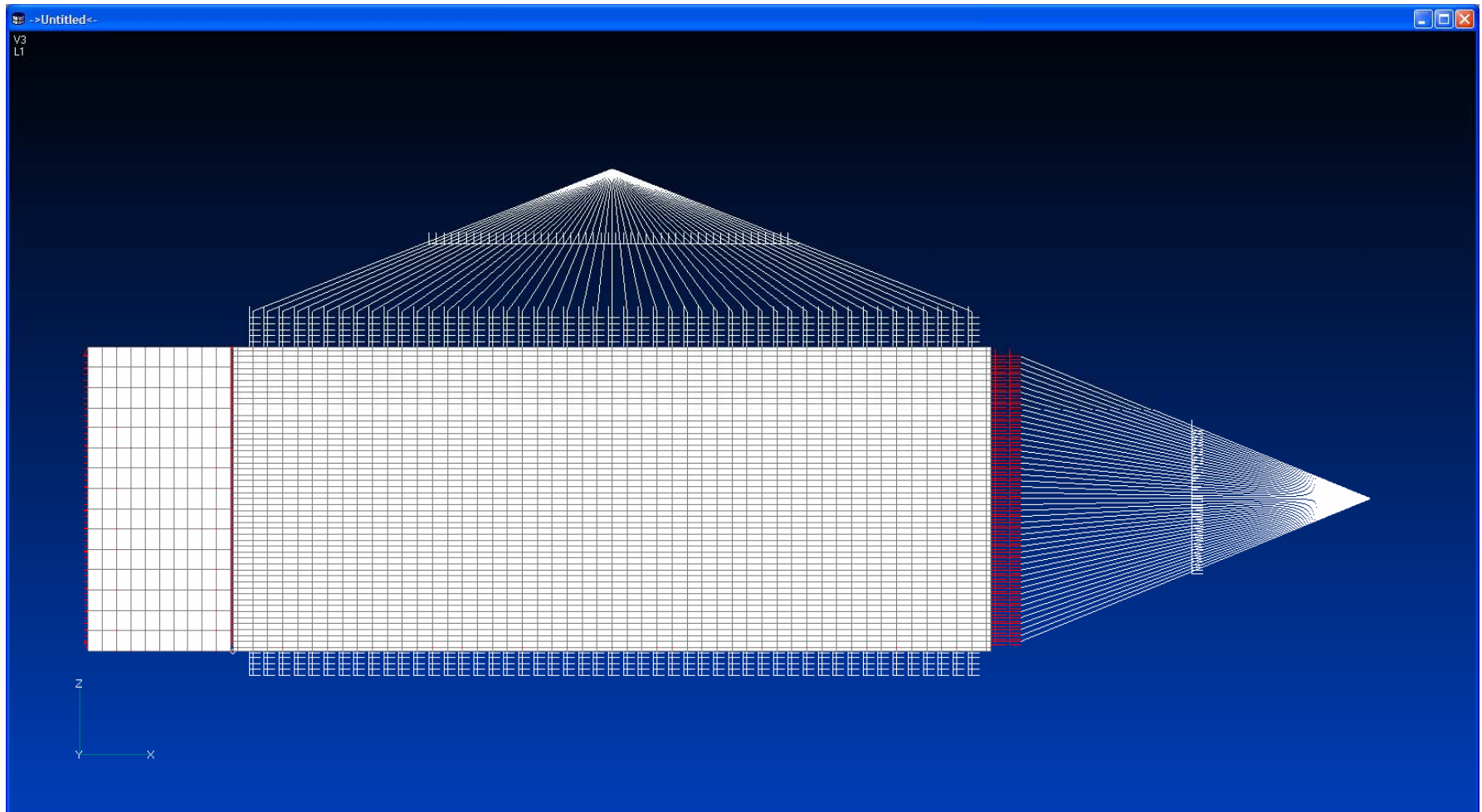
```
F CALL ARRAYMAKER(FILENM(1) , HAALL123) !All Hot Air Nodes.LST
F CALL ARRAYMAKER(FILENM(2) , HAL1 ) !Hot Air Nodes in HE in Layer 1.LST
...
c Construct the NGN arrays
F hot=.true.
F CALL MK(hot,HCL1,SHCL1,HP0L1,SHP0L1,HPLL1,SHPLL1,HP0L1NGN,
F &SHP0L1NGN,HPLL1NGN,SHPLL1NGN,HC0L1NGN,SHC0L1NGN,HCLL1NGN,
F &SHCLL1NGN)
...
c Construct Triplet arrays
F CALL TRIPMAKR(HC0L1NGN,SHC0L1NGN,HCLL1NGN,SHCLL1NGN,HCL1T,SHCL1T)
F PRINT*,"TRIPLET1"
...
F hot=.true. !update conductors from partings to hot air
F print*,"hot", hot
F DO I=1,SHPL1T
F DO J=2,4,2
F CALL Gconv(hhotL1,hot,G(HPL1T(I,J)),G(HPL1T(I,J)))
F ENDDO
F ENDDO
...
F100 CONTINUE !Update hot layer heats
F hot=.true.
F CALL Qfin(HPL1T,SHPL1T,hhotL1,hot)
F CALL Qfin(HCL1T,SHCL1T,hhotL1,hot)
...
F IF( (TIMEO > Timenot).AND.(TIMEO < Timenot+Tau)) THEN
F DO J=1,SALLHOTG
F G(ALLHOTGN(J))=0.0 !close all hot conductors
F ENDDO
```

The average exit air temperature is computed by constructing one-way conductors from nodes at the exit to a single node, the Averaging Node. (Elements were constructed by using **Closest Link** under meshing menu).

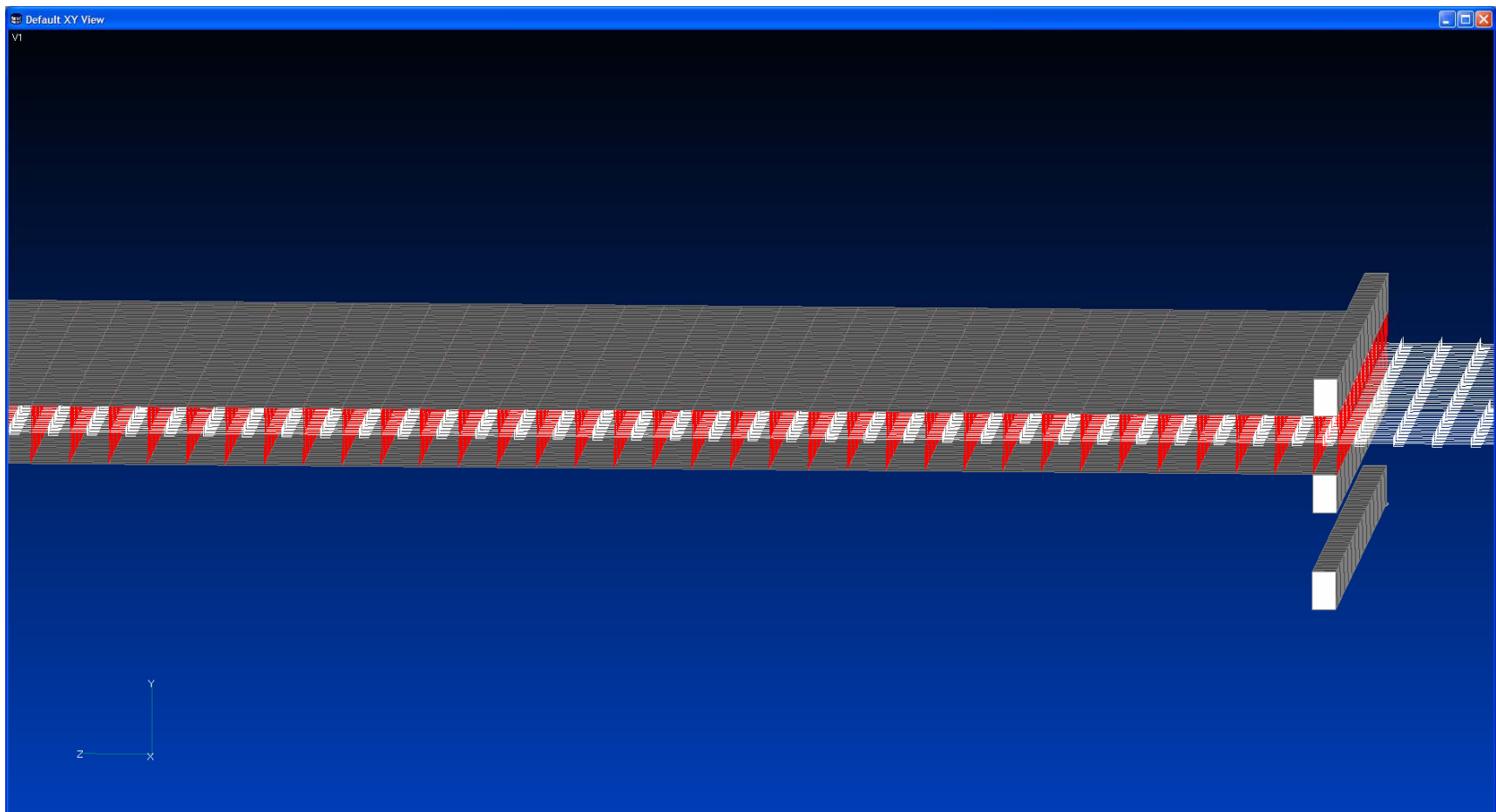




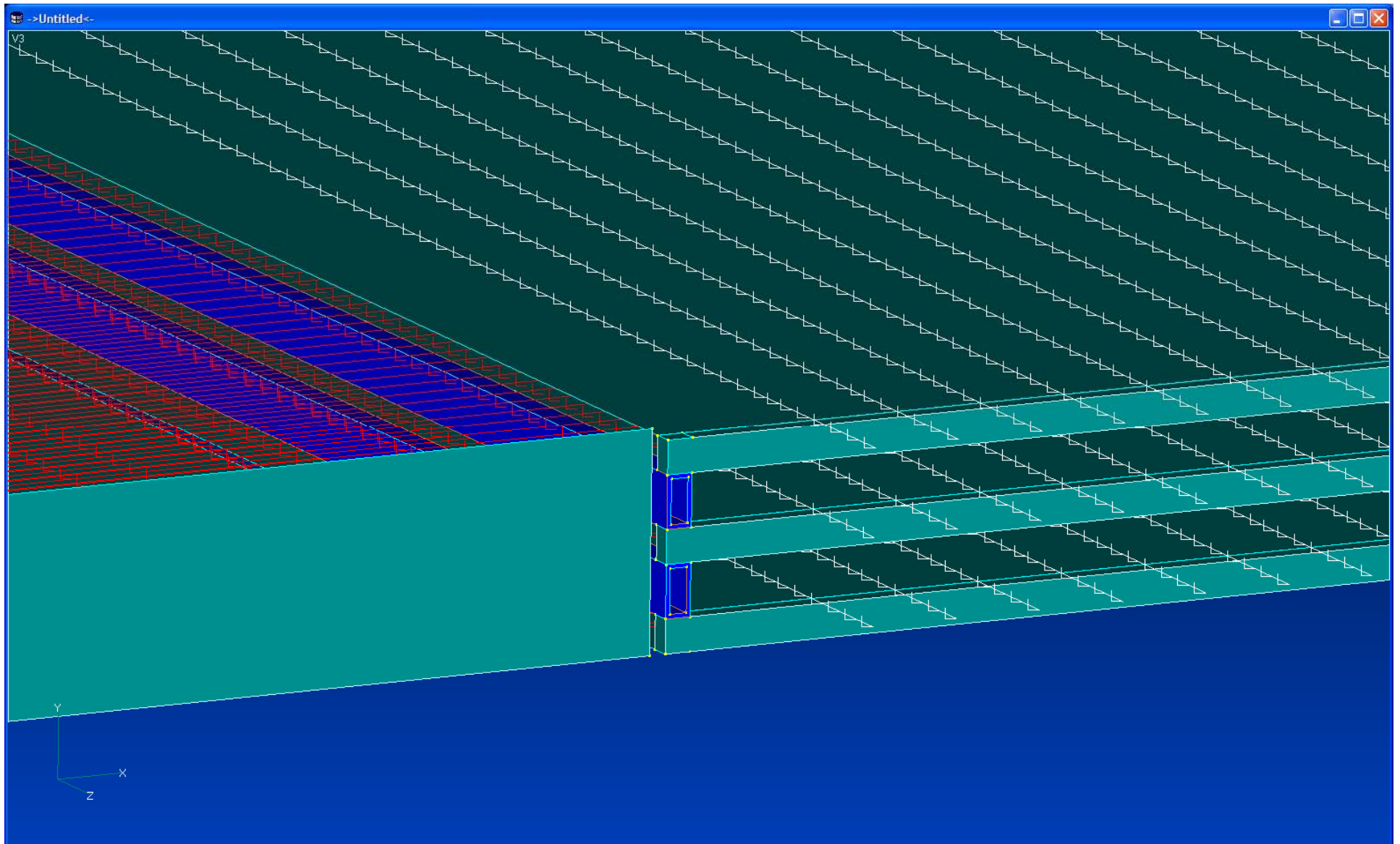
# Heat Exchanger with One-Way Conductors to Averaging Nodes



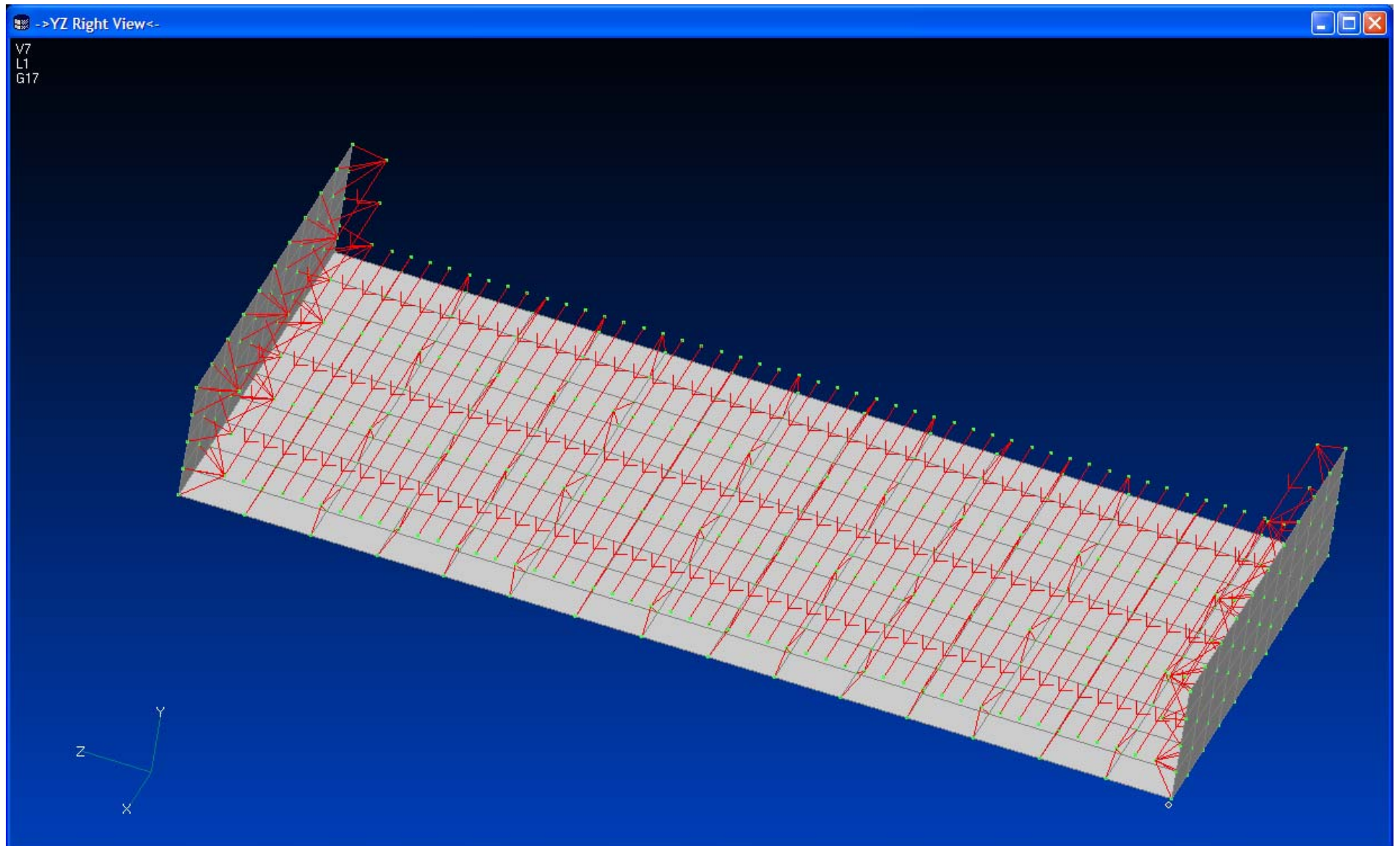
Convection conductors (shown in red) from air streams to parting plates were constructed by using the Contact Segments Algorithm.



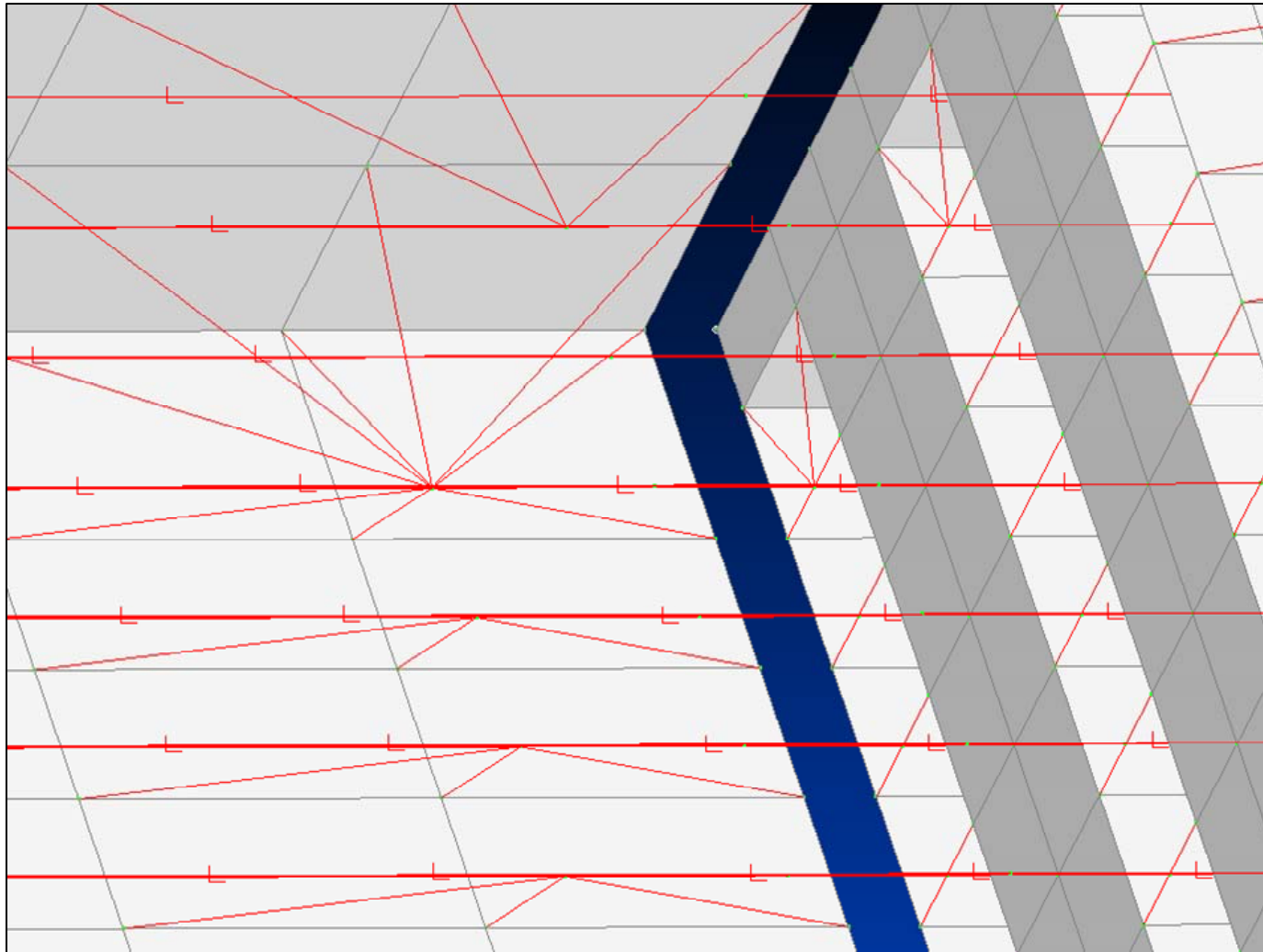
# Hot and Cold Air Flow Through Ducts



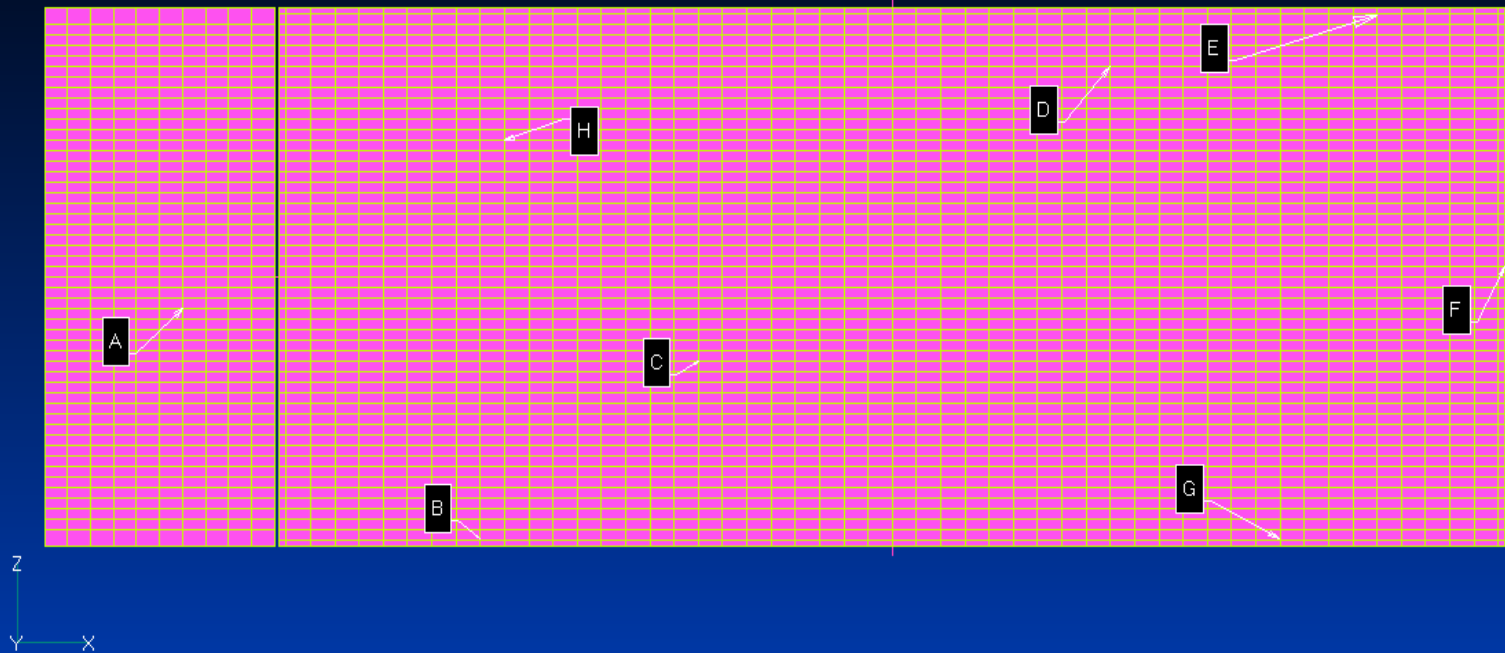
# Header with Conductors to Air Streams



Corner of Header near hot air inlet showing contact conductors and one-way flow elements.

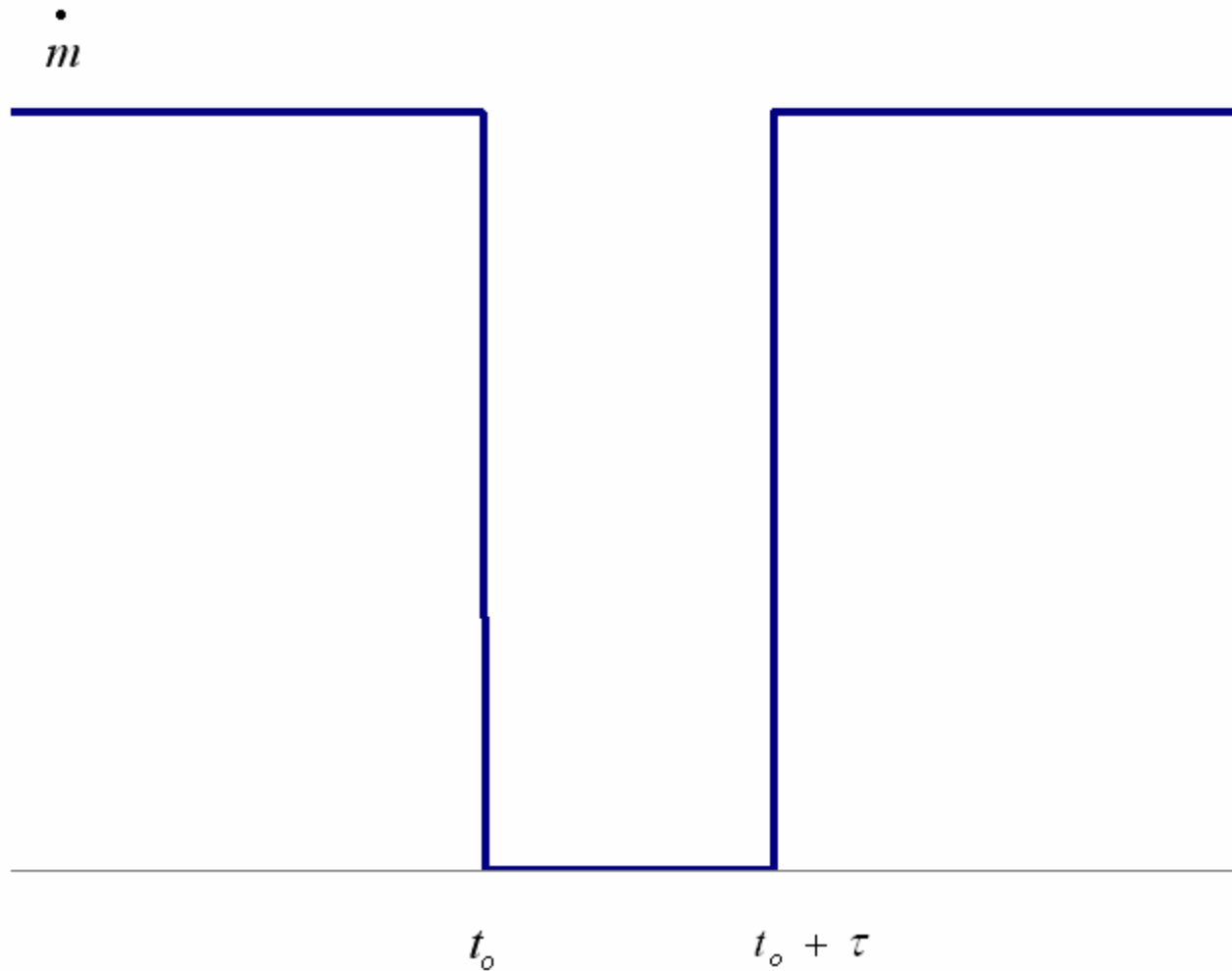


# Some Plotting Locations

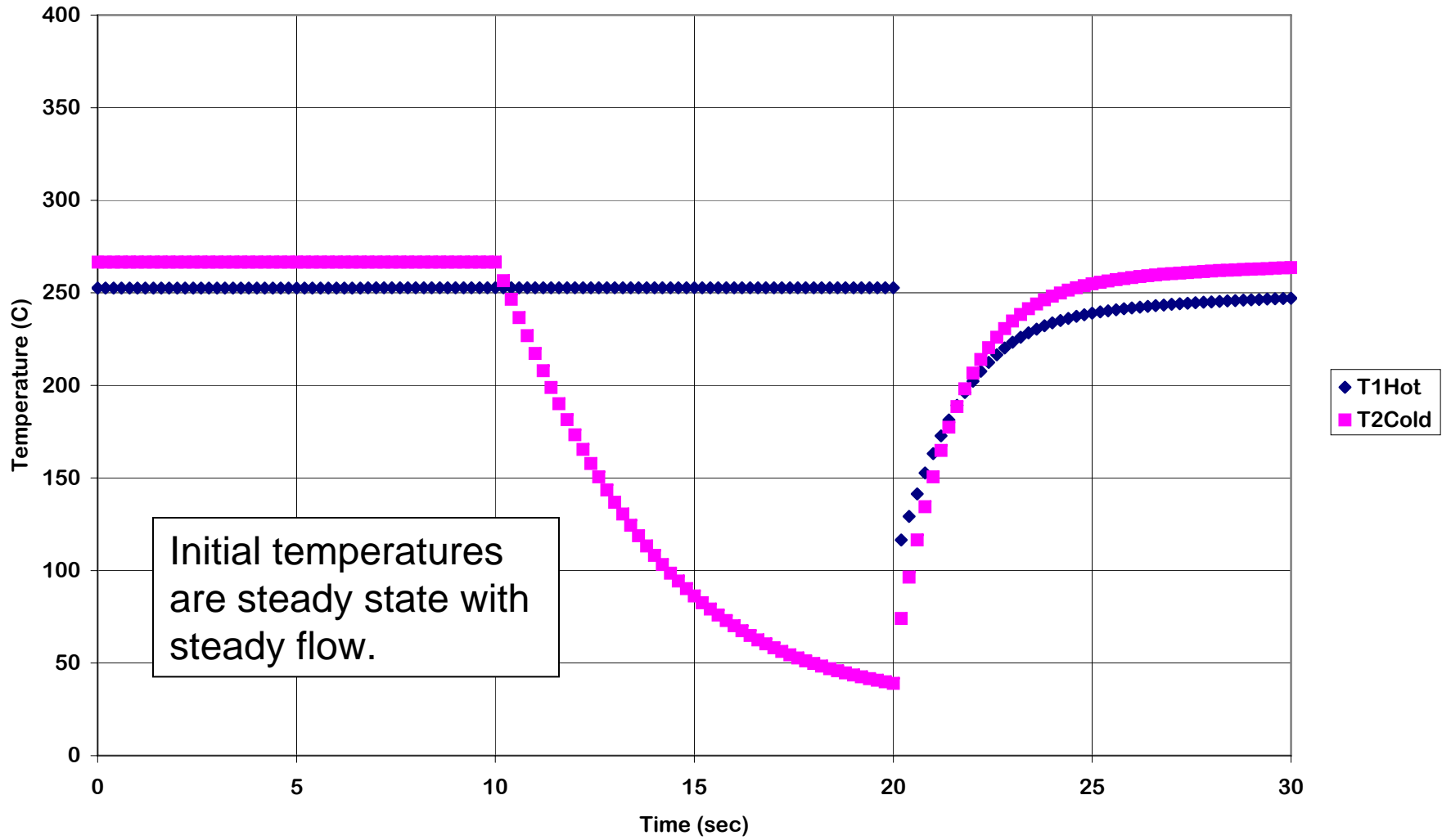


- Cold Air flows in z direction
- Hot Air flows in the x direction

# The Hot Air Stream is Pulsed

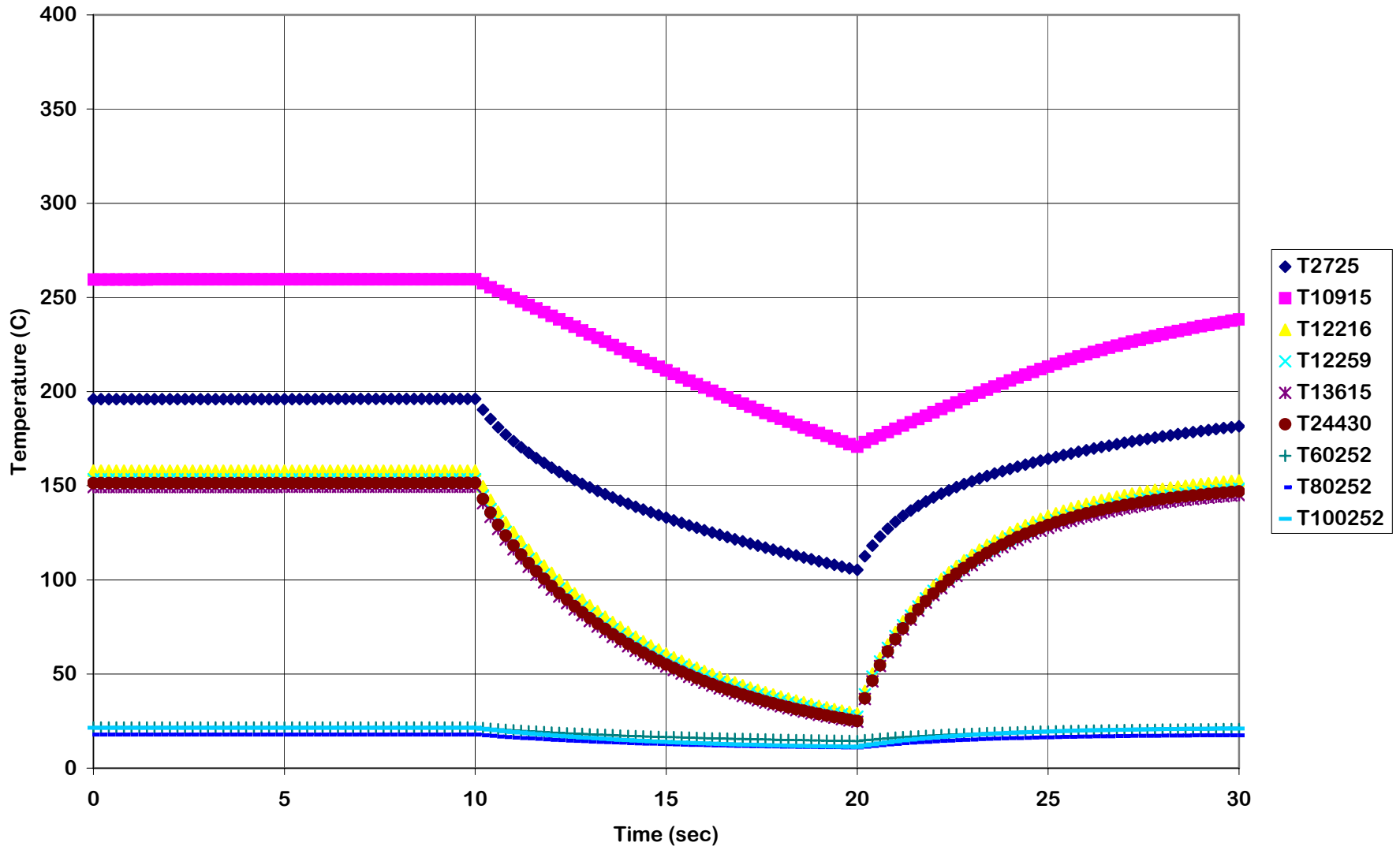


Average Exit Temperatures

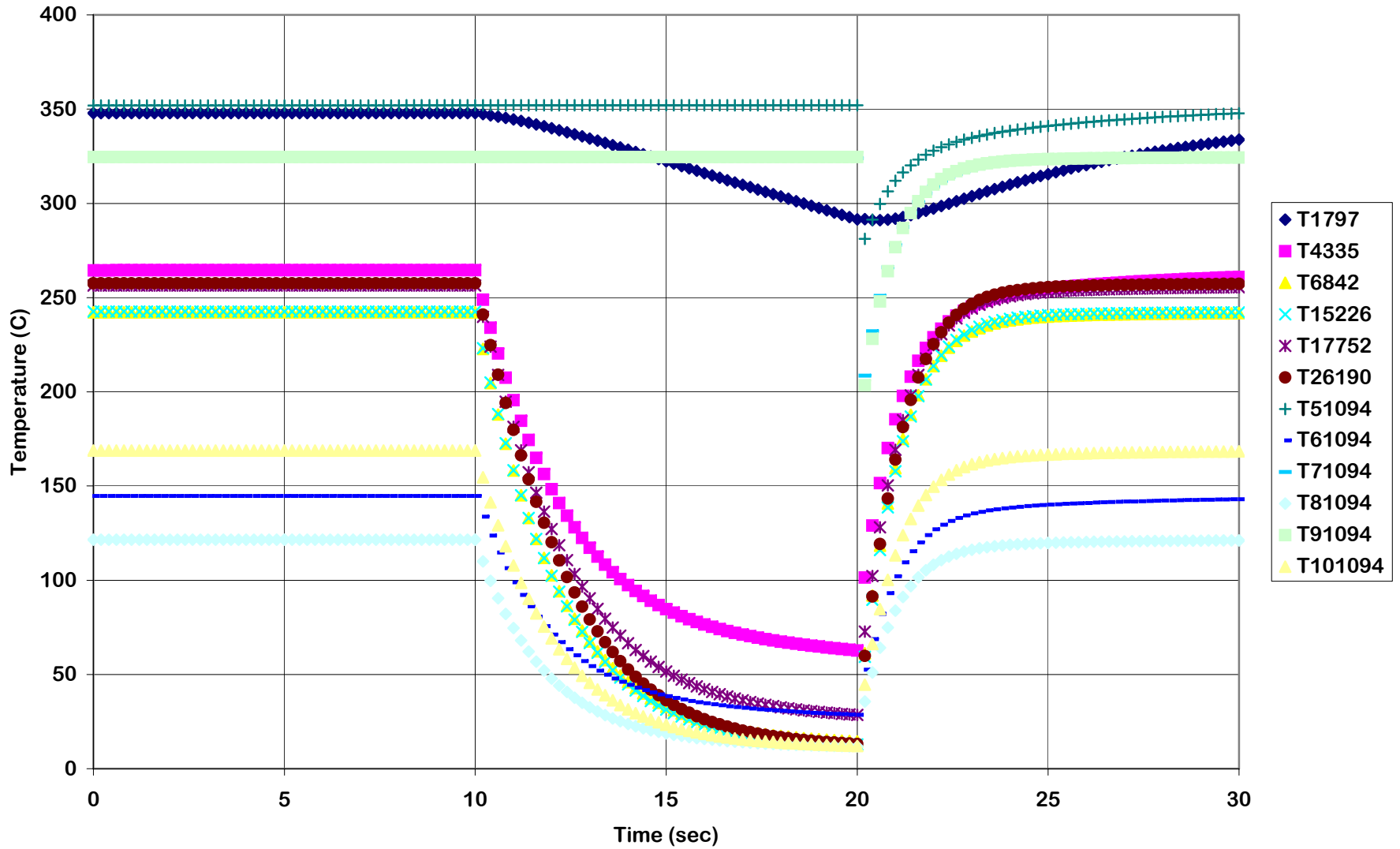




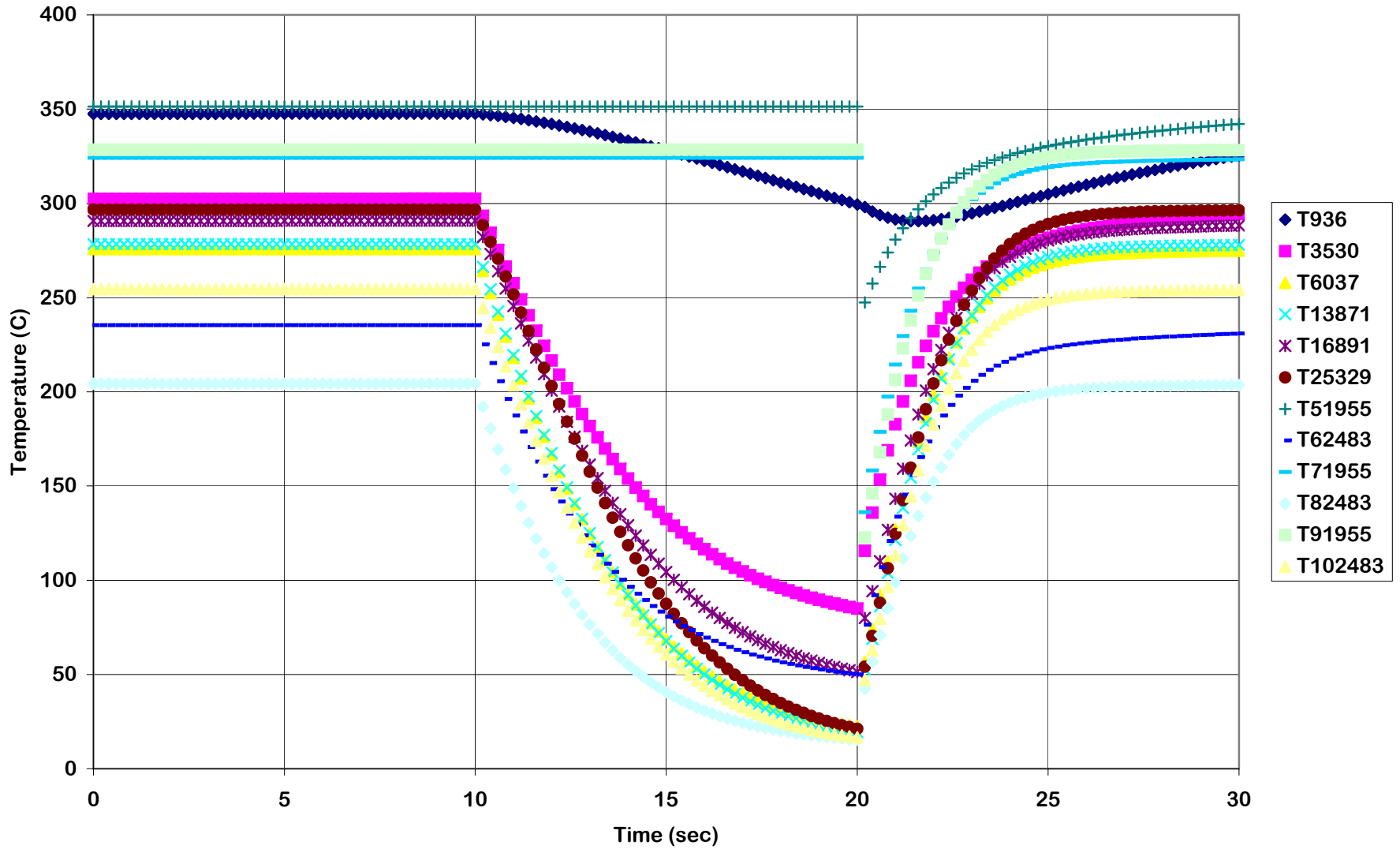
Location B



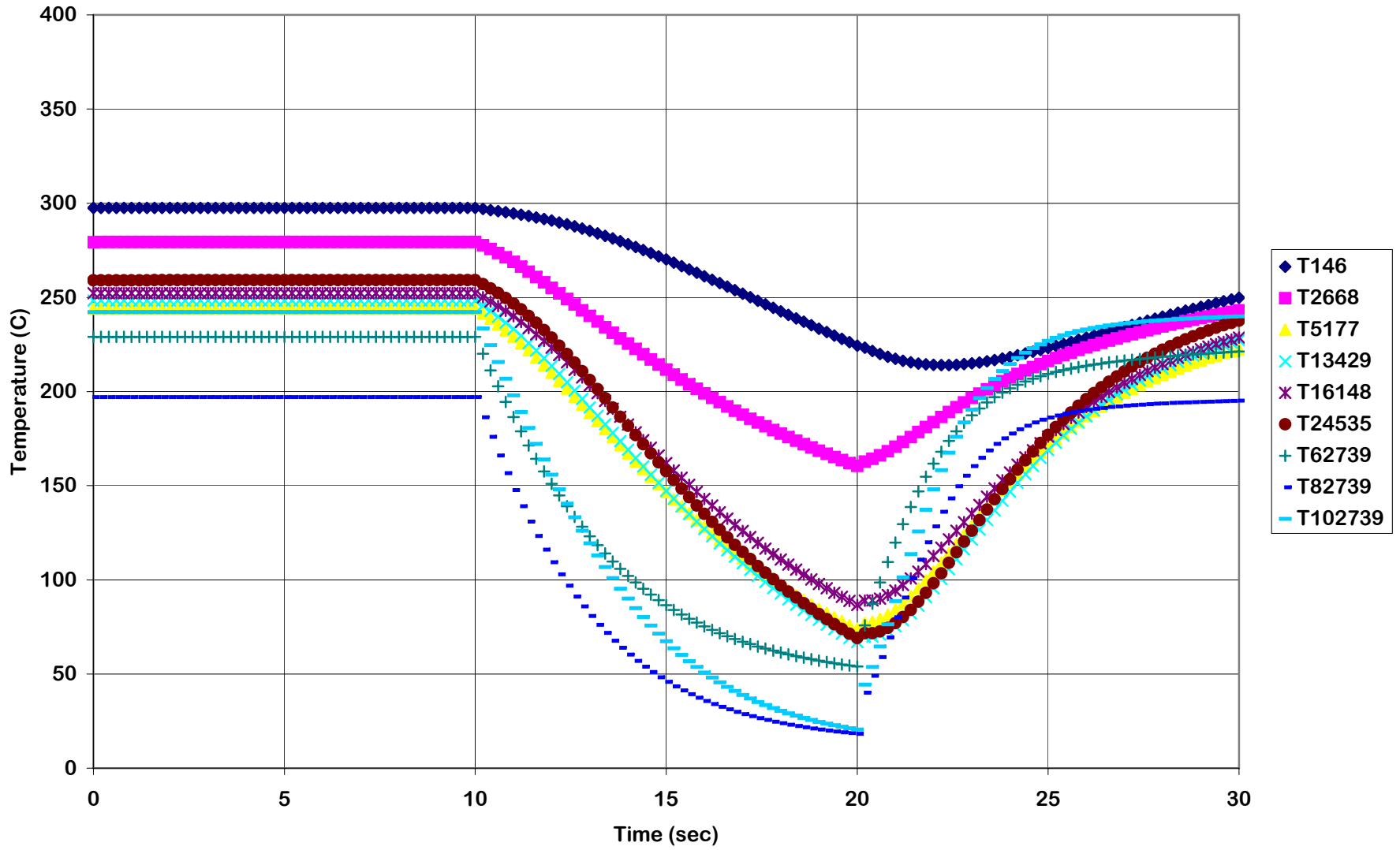
Location C



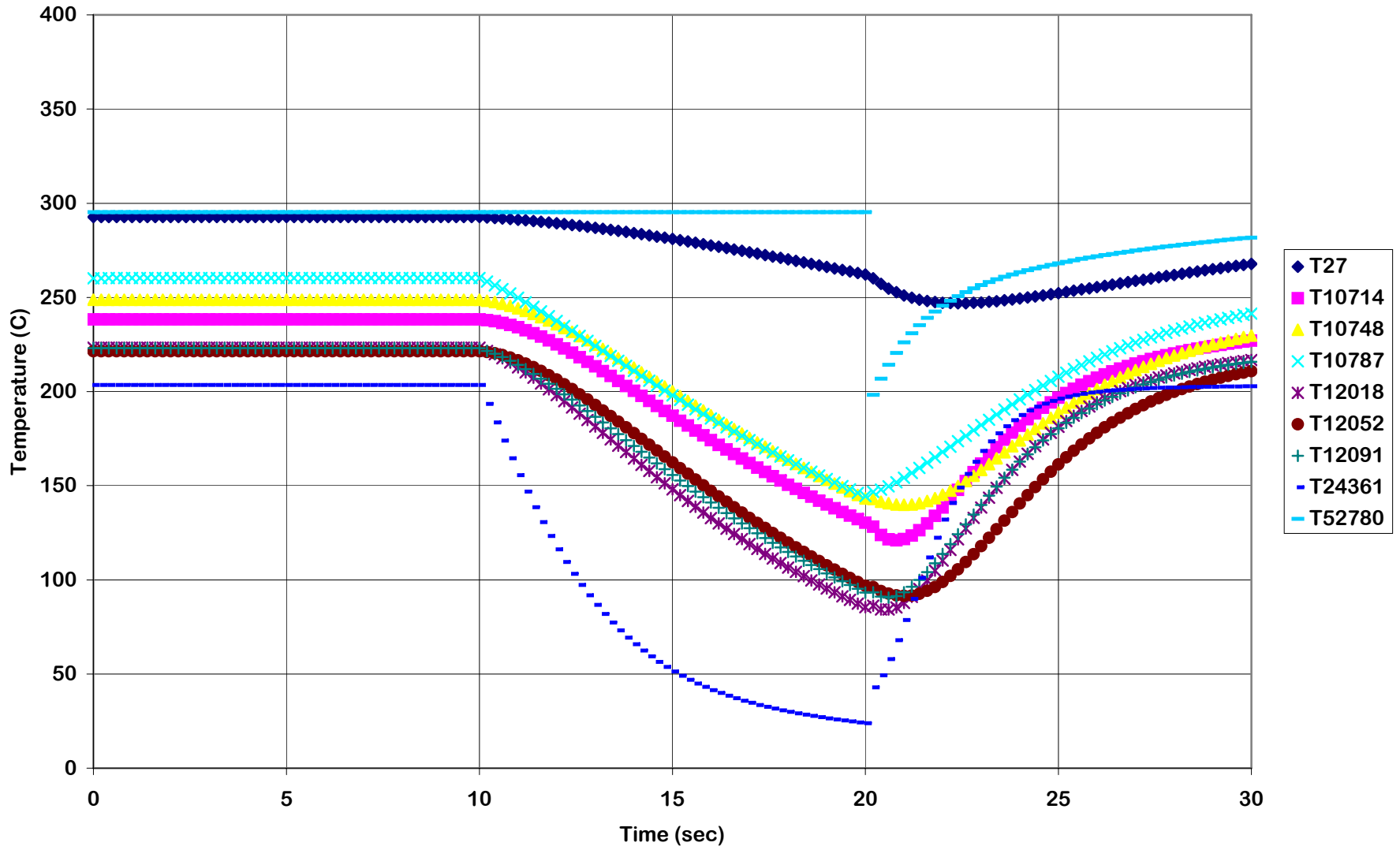
Location D



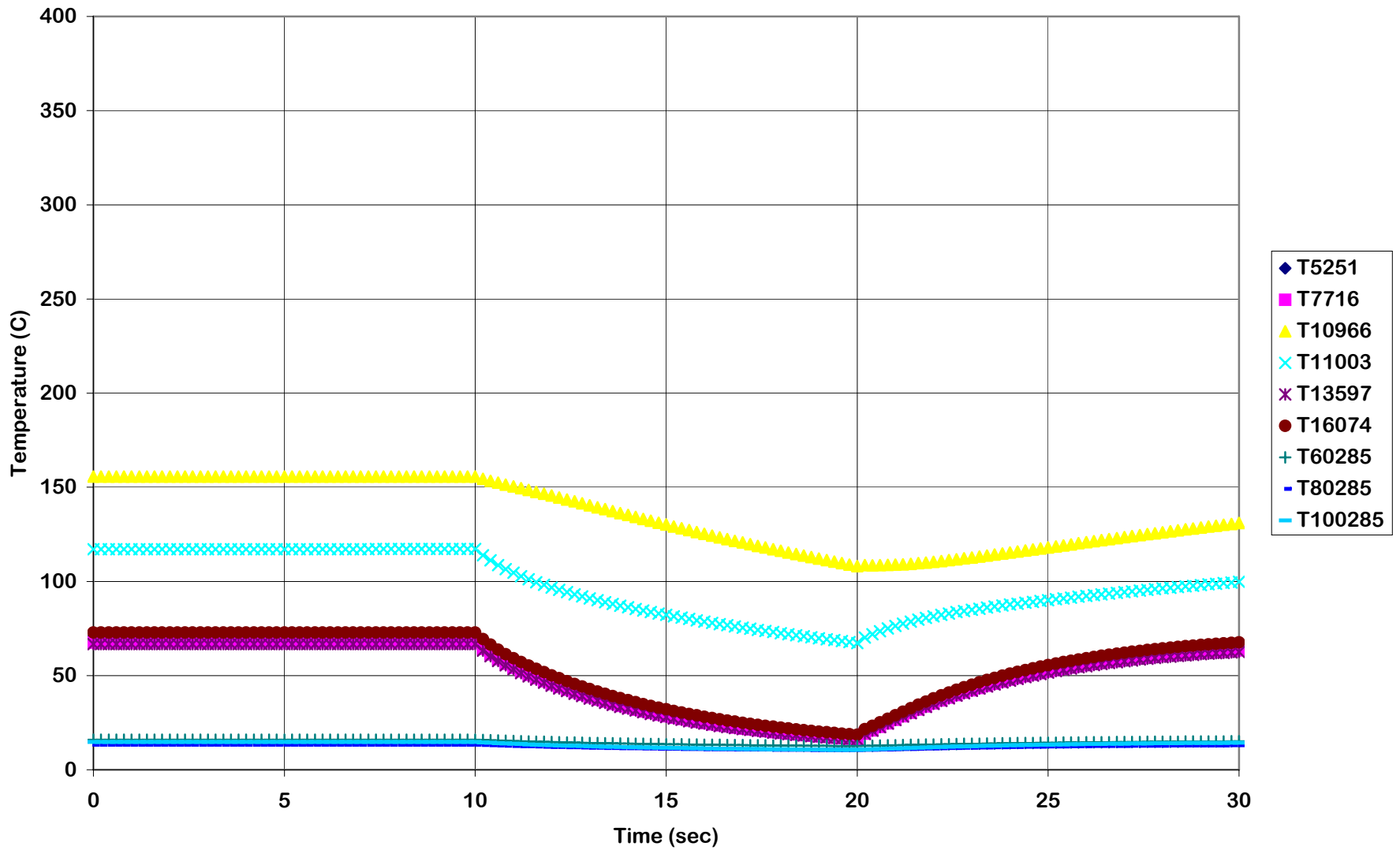
Location E



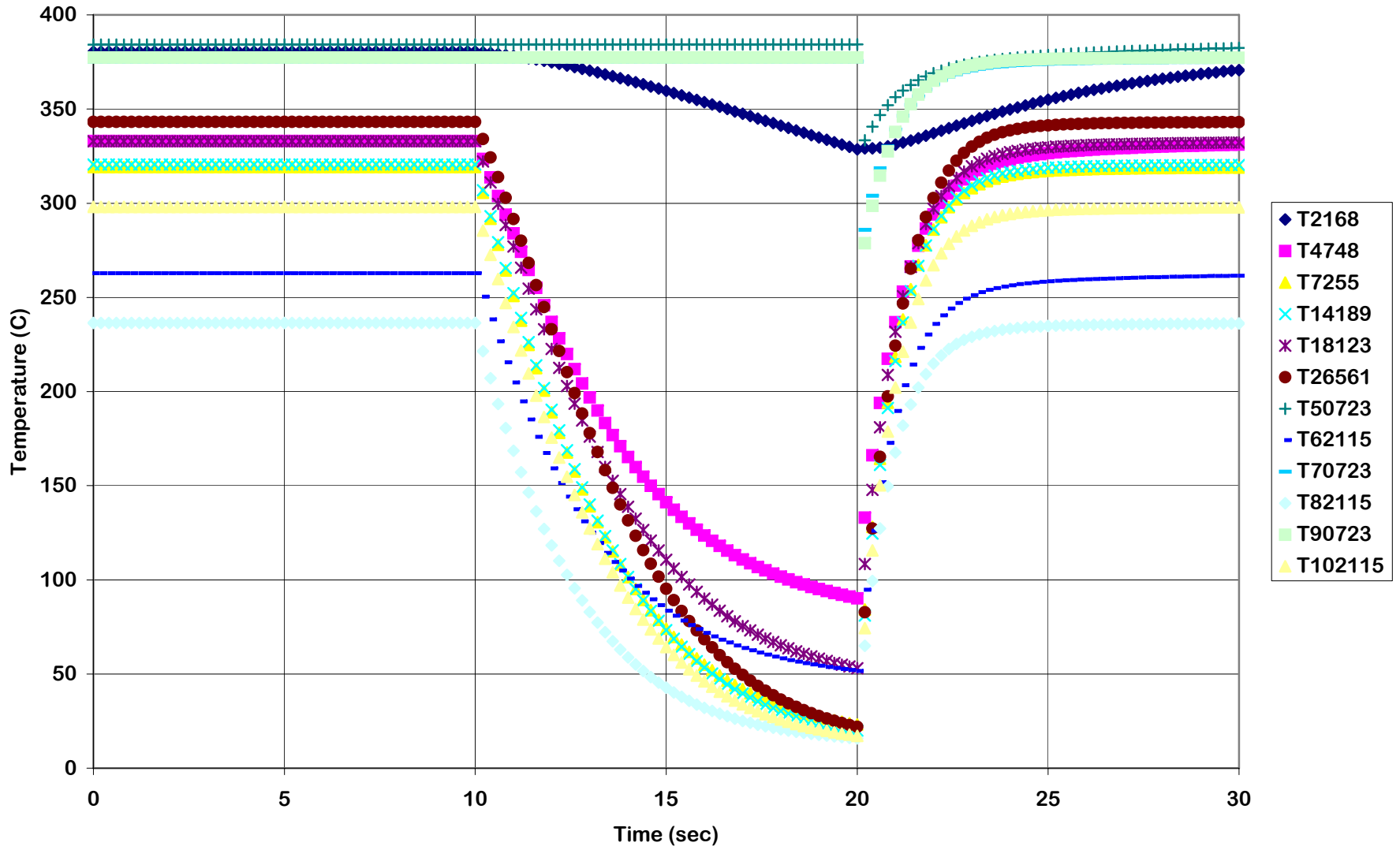
Location F



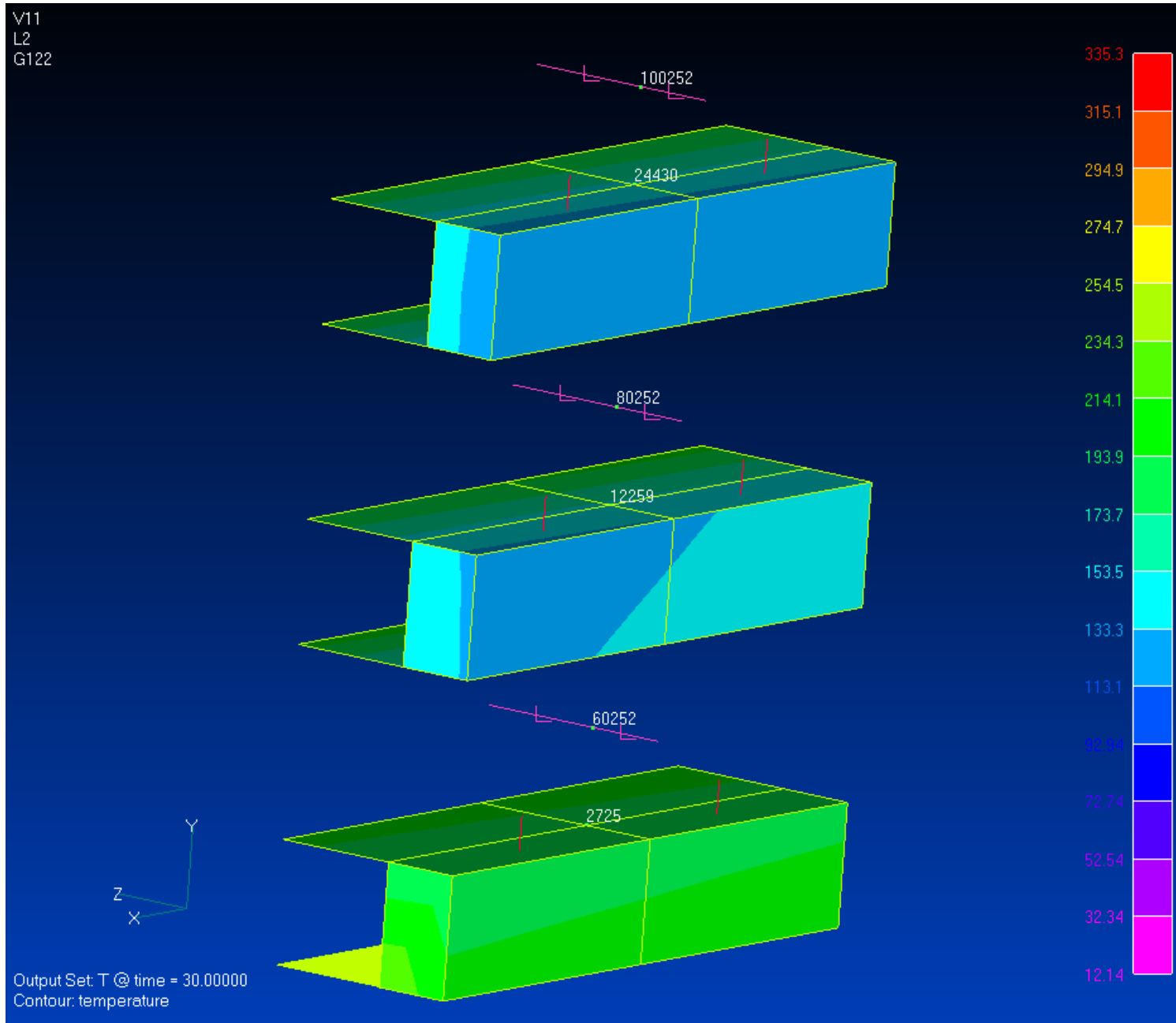
### Location G



Location H

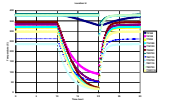
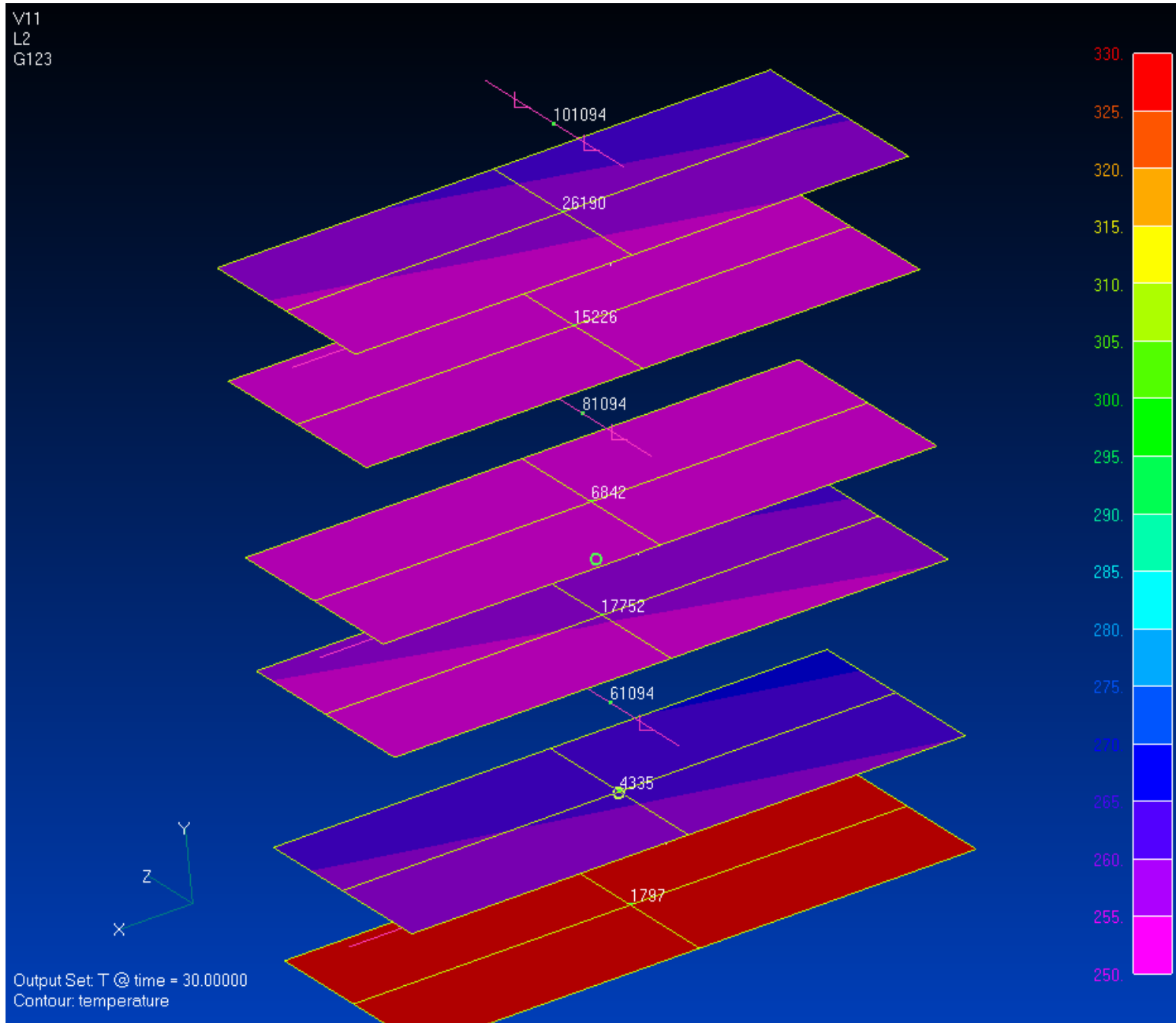


B

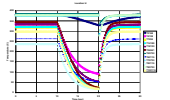
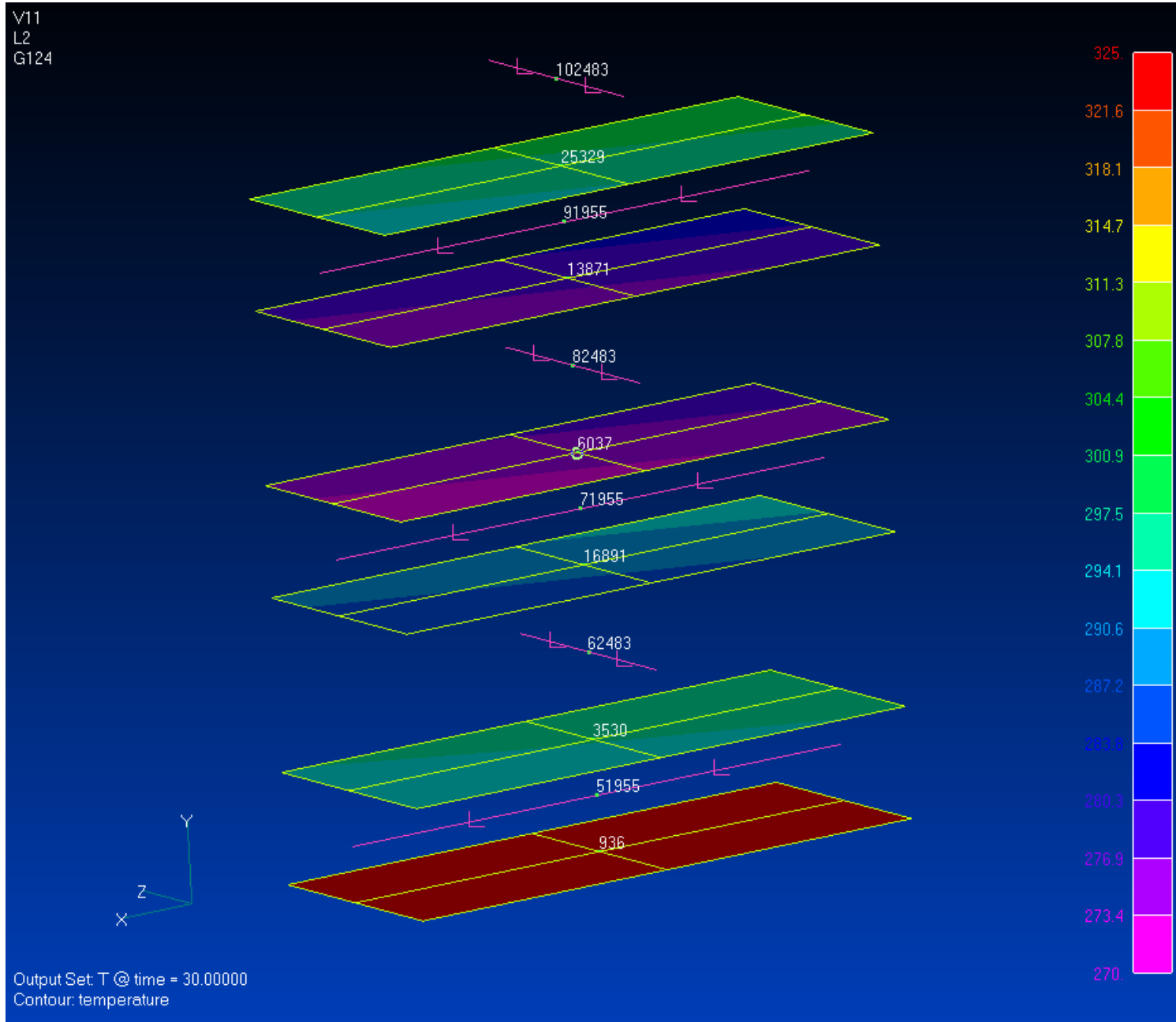




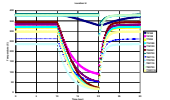
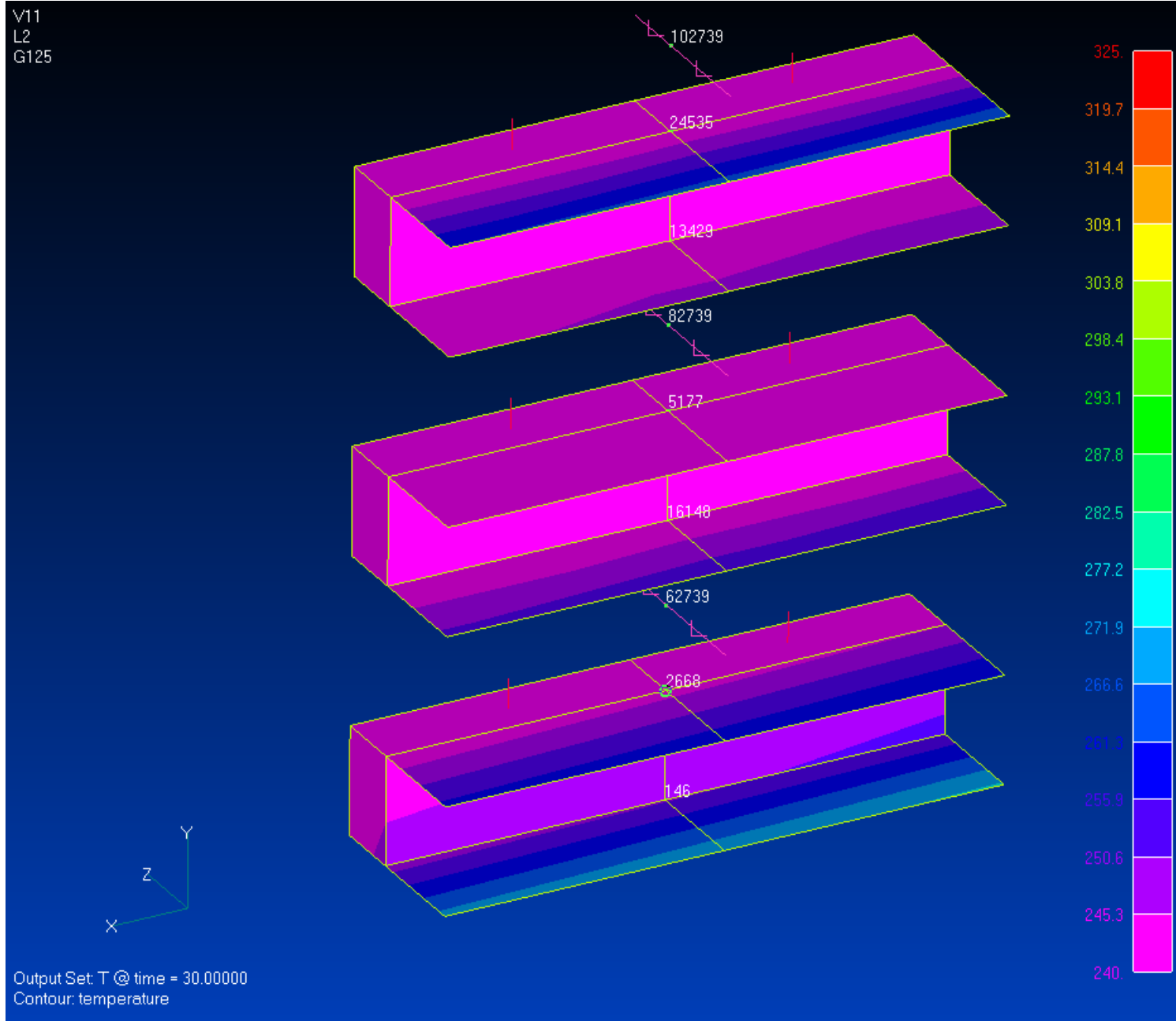
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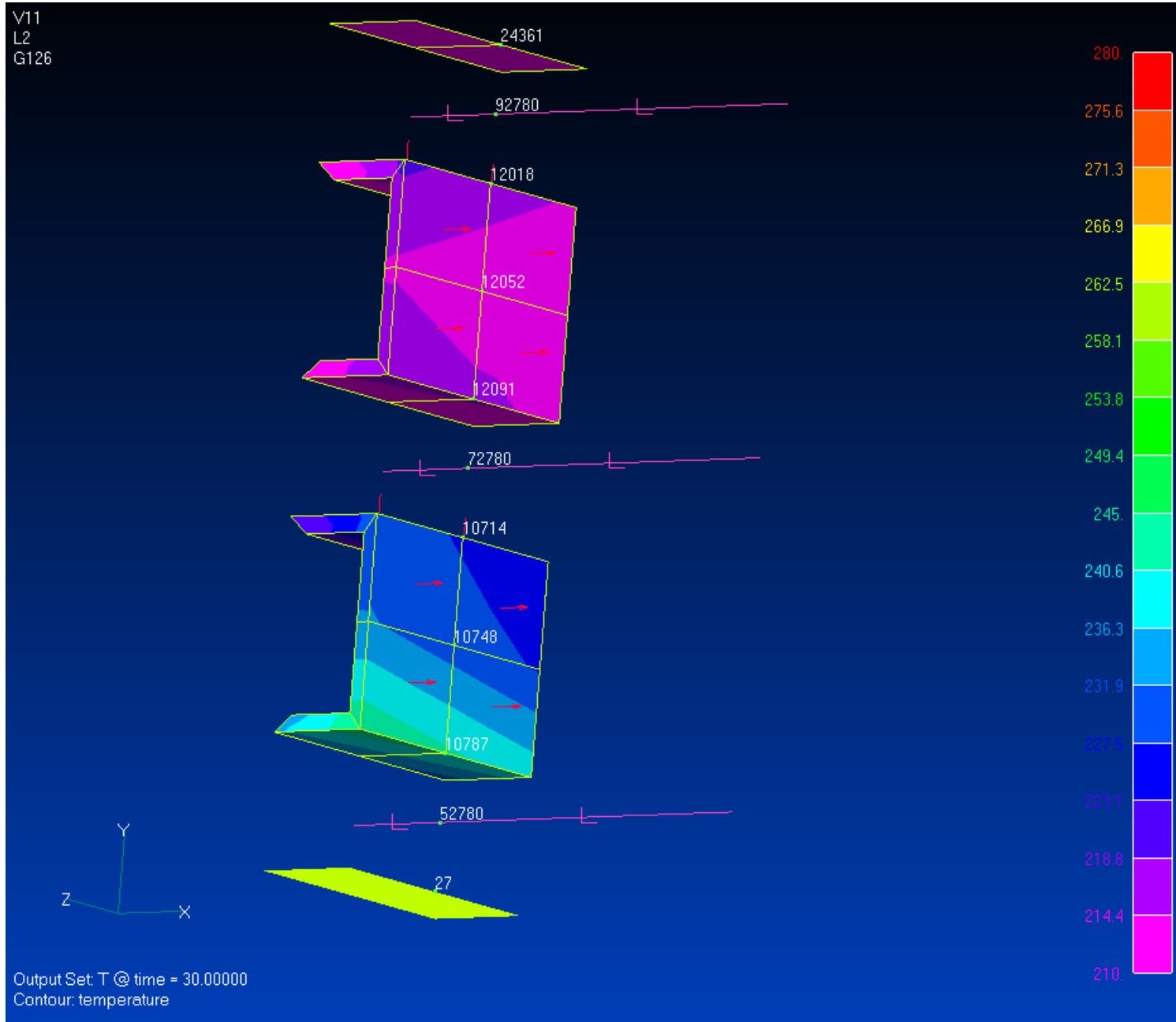
D



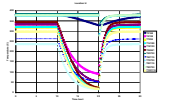
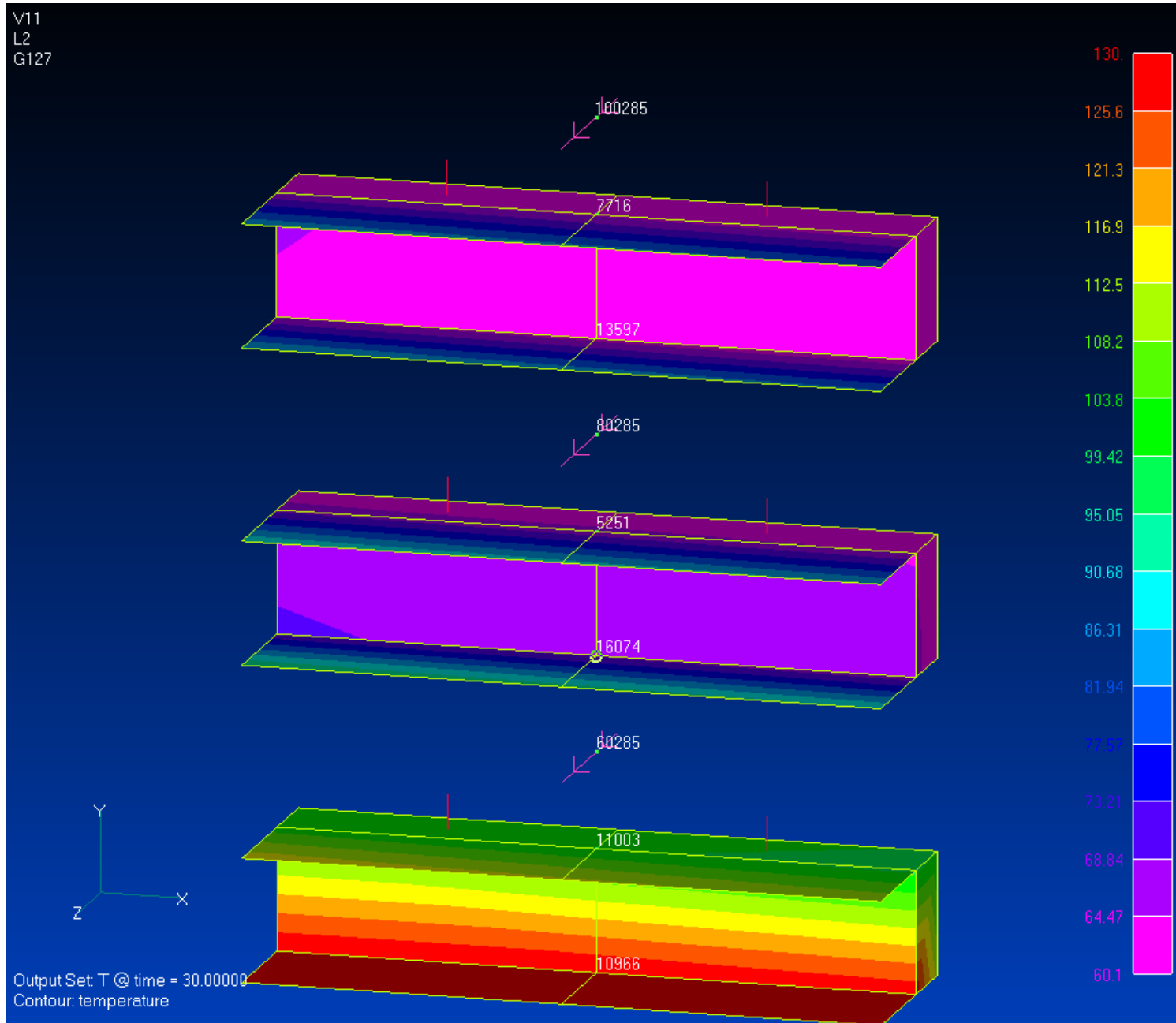
E



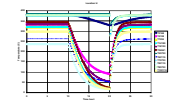
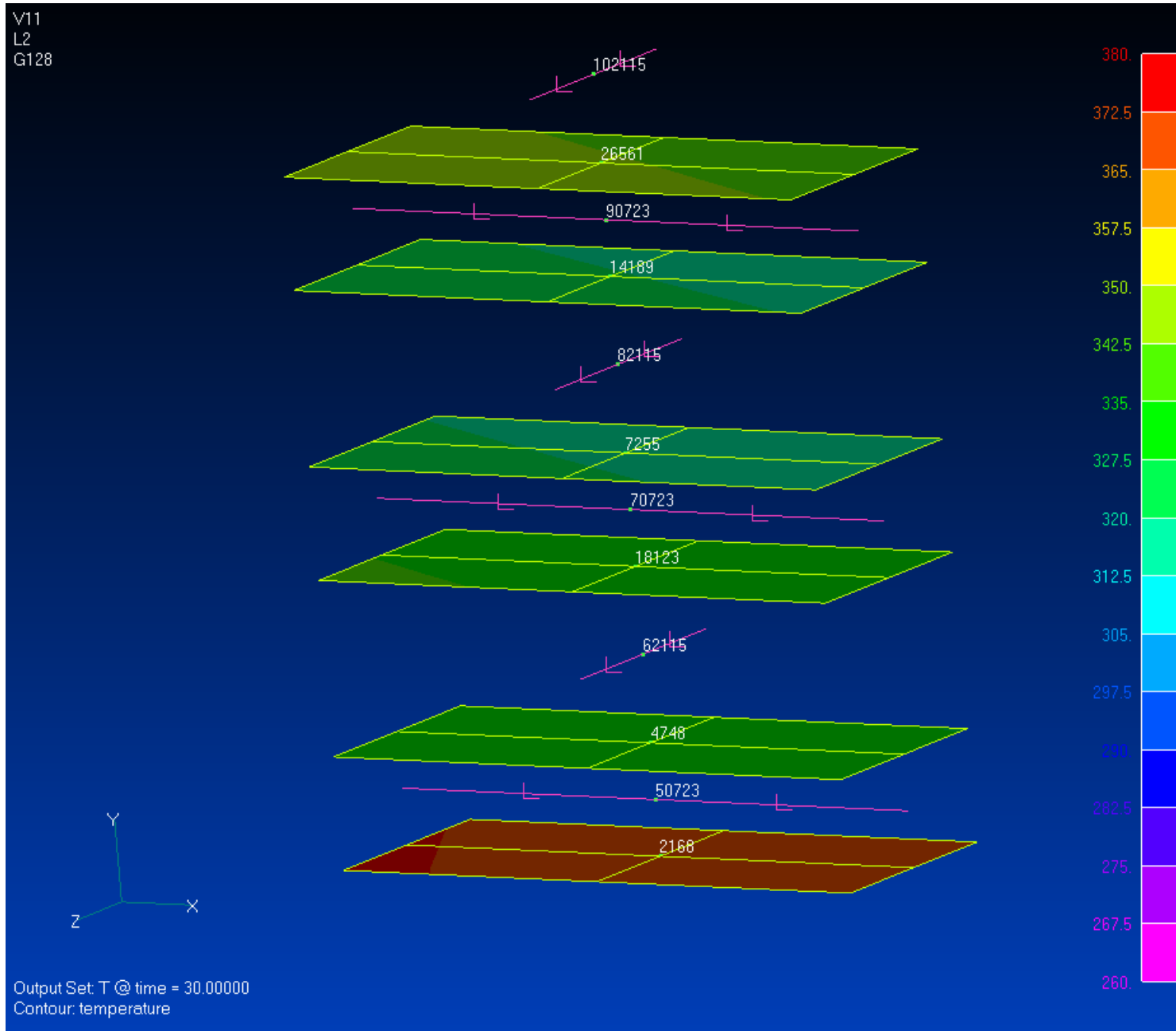
F



G



# H



# Letter of Appreciation for Phase 1



TAT Technologies Ltd.

To: Mr. Ron Behee,  
President of NETWORK ANALYSIS INC.  
Mr. John Pinckney  
Technical Support Manager

April 04, 2005

## Letter of Appreciation

We wish to express our heartfelt appreciation to Mr. John Pinckney for his assistance and support on the SINDA/FEMAP software we are using since 2002. We would like to mention the outstanding responsibility and professionalism of Mr. John Pinckney in carrying out the above activities.

TAT Technologies Ltd. is looking forward to closely cooperating with your company in the future.

Shlomo Ostersezer  
TAT Chairmen, CEO

Mark Shmurak  
Thermal Design Engineer